**PATENT** 

# COMPACT LOW NO<sub>x</sub> GAS BURNER APPARATUS AND METHODS

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# **BACKGROUND OF THE INVENTION**

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# 1. FIELD OF THE INVENTION.

The present invention relates to gas burner apparatus and methods for burning fuel gas-air mixtures whereby flue gases having low NO<sub>x</sub> content are produced.

# 2. DESCRIPTION OF THE PRIOR ART.

Emission standards are continuously being imposed by governmental authorities which limit the quantities of gaseous pollutants such as oxides of nitrogen (NO<sub>x</sub>) which can be emitted into the atmosphere. Such standards have led to the development of various improved gas burner designs which lower the production of NO<sub>x</sub> and other polluting gases. For example, methods and apparatus have been developed wherein all of the air and some of the fuel is burned in a first zone and the remaining fuel is burned in a second zone. In this staged fuel approach, an excess of air in the first zone acts as a diluent which lowers the temperature of the burning gases and thereby reduces the formation of NO<sub>x</sub>. Other methods and apparatus have been developed wherein flue gases are combined with fuel gas and/or fuel gas-air mixtures to dilute the mixtures and lower their combustion temperatures and the formation of NO<sub>x</sub>.

While the above described prior art methods and burner apparatus for producing flue gases having low NO<sub>x</sub> content have achieved varying degrees of success, there still remains a need for improvement in gas burner apparatus and methods of burning fuel gas whereby simple economical burner apparatus is utilized and low NO<sub>x</sub> content flue gases are produced. Further, the burner apparatus utilized heretofore to carry out the above described methods have generally been large, produce flames of long length and have low turn down ratios.

Thus, there are needs for improved burner apparatus and methods which produce low NO<sub>x</sub> content flue gases and the burner apparatus are compact, have short flame lengths and have high turn down ratios.

#### SUMMARY OF THE INVENTION

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By the present invention compact low NO<sub>x</sub> gas burner apparatus and methods are provided which meet the needs described above and overcome the deficiencies of the prior art. That is, the present invention provides improved gas burner apparatus and methods for discharging mixtures of fuel gas and air into furnace spaces wherein the mixtures are burned and flue gases having low NO<sub>x</sub> content are formed therefrom. In addition, the compact burner apparatus of this invention are smaller than most prior art burner apparatus, have high turn down ratios and produce short flame lengths.

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A compact gas burner apparatus of this invention is basically comprised of a housing having an open end attached to a furnace space and means for introducing a controlled flow rate of air into the housing attached thereto. A refractory burner tile is attached to the open end of the housing having an opening formed therein for allowing air to pass from the housing into the furnace space. The burner tile includes a wall surrounding the opening which extends into the furnace space and forms a mixing zone within and above the wall. The exterior sides of the wall are divided into sections by a plurality of radially positioned baffles attached thereto with alternate sections having the same or different heights and slanting towards the opening at the same or different angles. Some or all of the sections, preferably every other section, have passageways formed therein for conducting primary fuel gas from outside the sections to within the wall. A primary fuel gas nozzle connected to a source of fuel gas can optionally be positioned within the opening and wall of the burner tile for mixing additional primary fuel gas with the air flowing through the burner tile. One or more fuel gas nozzles, preferably one for each external slanted wall section, connected to a source of fuel gas and positioned outside the wall of the burner are provided for discharging secondary fuel gas adjacent to one or more of the sections. One or more of the fuel gas nozzles, preferably every other fuel gas nozzle, also discharge primary fuel gas and flue gases into and through the primary fuel gas passageways whereby the secondary fuel gas mixes with flue gases in the furnace

space, the mixture of secondary fuel gas and flue gases mixes with unburned air, primary fuel gas and flue gases flowing through the opening and wall of the burner tile and the resultant mixture is burned in the furnace space in a folded flame pattern.

By the improved methods of the present invention a mixture of fuel gas and air is discharged into a furnace space wherein the mixture is burned in a folded flame pattern and flue gases having low NO<sub>x</sub> content are formed therefrom. A method of this invention basically comprises the steps of discharging the air into a mixing zone within and adjacent to a wall which extends into the furnace space and has exterior sides divided into alternating sections by a plurality of radially positioned baffles attached thereto. The alternating sections have the same or different heights and slant towards the opening at the same or different angles. One or more of the sections, preferably every other section of the alternating sections, have passageways formed therein for conducting a primary fuel gas and flue gases mixture from outside the sections to within the wall. A primary portion of the fuel gas is discharged from locations outside the wall and adjacent to the one or more wall sections having passageways formed therein so that the primary portion of the fuel gas is mixed with flue gases in the furnace space and the resulting primary fuel gas-flue gases mixture formed flows into the mixing zone within the wall by way of the one or more passageways to form a primary fuel gas-flue gases-air mixture which flows into the furnace space. Simultaneously, a secondary portion of the fuel gas is discharged from one or more locations outside the wall and adjacent to one or more of the wall sections so that the secondary portion of fuel gas mixes with flue gases in the furnace space and the secondary fuel gas-flue gases mixture formed is discharged into the primary fuel gas-flue gases-air mixture in a plurality of separate streams which enter and mix with the primary fuel gas-flue gases-air mixture to form a highly mixed fuel gas-flue gases-air mixture which burns in a folded flame pattern.

The objects, features and advantages of the present invention will be readily apparent to those skilled in the art upon a reading of the description of preferred embodiments which follows when taken in conjunction with the accompanying drawings.

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#### BRIEF DESCRIPTION OF THE DRAWINGS

FIGURE 1 is a perspective view of the burner tile of the present invention which includes a wall divided into sections by a plurality of radial baffles with alternate sections having different heights and slanting towards the opening at different angles.

FIGURE 2 is a side cross-sectional view of the burner apparatus of the present invention attached to a furnace wall including the burner tile of FIG. 1 with the view of the burner tile being taken along line 2-2 of FIG. 1.

FIGURE 3 is a top view of the burner of FIG. 2 taken along line 3-3 of FIG. 2. FIGURE 4 is a side cross-sectional view of the burner tile taken along line 4-4 of FIG. 3.

FIGURE 5 is a picture of the folded flame pattern produced by the burner apparatus and methods of this invention.

#### **DESCRIPTION OF PREFERRED EMBODIMENTS**

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Referring now to the drawings, a compact, low NO<sub>x</sub>, gas burner apparatus of the present invention is illustrated and generally designated by the numeral 10. As best shown in FIG. 2, the burner apparatus 10 is sealingly attached to the bottom wall 12 of a furnace space over an opening therein. While gas burner apparatus are commonly mounted vertically and fired upwardly as shown in FIG. 2, it is to be understood that the burner apparatus can also be mounted horizontally and fired horizontally or vertically and fired downwardly. The burner apparatus 10 is comprised of a housing 14 having an open end 16 and an open end 18. The housing 14 is attached to the furnace wall 12 by means of a flange 20 and a plurality of bolts 22 which extend through complimentary openings in the flange 20 and the wall 12. An air flow rate regulating register 24 is connected to the housing 14 at its open end 16 for regulating the flow rate of combustion air entering the housing 14. The furnace wall 12 includes an internal layer of insulating material 26 attached thereto, and the open end 18 of the housing 14 includes a burner tile 28 formed of flame and heat resistant refractory material attached thereto. As illustrated in FIG. 2, the interior surface of the insulating material 26 attached to the furnace wall 12 and the top of the base portion 30 of the burner tile 28 define a furnace space within which the fuel gas

and air discharged by the burner apparatus 10 are burned. The burner tile 28 has a central opening 32 formed in the base portion 30 thereof through which air introduced into the housing 14 by way of the air register 24 is discharged. The burner tile 28 also includes a wall portion 34 which surrounds the opening 32 and extends into the furnace space. The burner tile 28, the interior of the wall portion 34 and the central opening 32 in the base portion 30 of the burner tile 28 as well as the housing 14 can take various shapes, e.g., circular, rectangular, square, triangular, polygonal or other shape. However, the burner apparatus 10 preferably includes a circular burner tile 28 having a circular opening 32 therein and a circular wall portion 34. Also, the housing 14 preferably includes a circular opening 18 therein and the housing is preferably cylindrical. However, the housing can also include a square opening 18 therein and can have square or rectangular sides 15. In a preferred embodiment as shown in FIG. 2, the opening 32 in the burner tile 28 is smaller than the interior sides 33 of the wall 34 thereof so that a ledge 35 is provided within the tile 28 which functions as a flame stabilizing surface.

Referring now to FIG. 1, a perspective view of the burner tile 28 and the wall 34 thereof is shown. The interior sides of the wall 34 are vertical as best shown in FIG. 2. The exterior sides of the wall 34 are divided into a plurality of sections 36 and 38 by radially positioned baffles 40 with the alternate sections 36 and 38 having the same or different heights and slanting towards the opening 32 at the same or different angles. Preferably, the alternating sections have different heights and slant at different angles as shown in the drawings.

Referring now to FIG. 4, it can be seen that in a preferred embodiment the sections 36 have short heights and slant towards the opening 32 in the burner tile 34 at large angles as compared to the sections 38 which have taller heights and slant toward the opening 32 at smaller angles. As will now be understood and as shown in FIGS. 1-4, the sections 36 and 38 between the baffles 40 alternate around the wall 34. In the embodiment illustrated in the drawing, there are four of the sections 36 and four of the sections 38. Depending on the size of the burner, there can be more or less of the alternating sections with the totals being even numbers, e.g., 4, 6, 8, 10, etc.

The alternating sections 36 have heights in the range of from about 0 inches to about 16 inches and slant towards the opening 32 at an angle in the range of from about 0 degrees to about 90 degrees. The alternating sections 38 can have the same or different heights as the alternating sections 36 in the range of from about 2 inches to about 16 inches and slant towards the opening 32 at the same or different angles in the range of from about 0 degrees to about 60 degrees. Preferably, the alternating sections 36 have heights in the range of from about 0 inches to about 16 inches and slant in the range of from about 0 degrees to about 90 degrees and the alternating sections 38 have different heights in the range of from about 2 inches to about 16 inches and slant differently in the range of from about 0 degrees to about 60 degrees. As shown best in FIGS. 2-4, the sections 36 each include a passageway 42 extending from the outside to the inside of the wall 34 through which fuel gas mixed with flue gases flow as will be described further hereinbelow.

In a more preferred arrangement of the alternating sections 36 and 38, the first of the alternating sections have heights in the range of from about 5 inches to about 10 inches and slant towards the opening at an angle in the range of from about 10 degrees to about 30 degrees, and the second of the alternating sections have the same or different heights as the first of the alternating sections in the range of from about 6 inches to about 12 inches and slant towards the opening at the same or different angles in the range of from about 5 degrees to about 15 degrees.

In a presently preferred arrangement, the first of the alternating sections have heights of about 7 inches and slant towards the opening at an angle of about 20 degrees, and the second of the alternating sections have heights of about 9 inches and slant towards the opening at an angle of about 10 degrees.

As shown in FIGS. 1 and 2, a central primary fuel gas nozzle 44 can optionally be positioned within the opening 32 near the bottom of the burner tile 28. When used, the nozzle 44 is connected by a conduit 46 to a fuel gas manifold 48. The conduit 46 is connected to the manifold 48 by a union 50 and a conduit 52 connected to the manifold 48 is connected to a source of pressurized fuel gas. As shown in FIGS. 2 and 3, a venturi 37 can optionally be positioned around and above the nozzle 44 so that a fuel gas lean mixture of fuel gas and air is formed and combusted in and

above the venturi 37. Also, the burner 14 can optionally include a plurality of nozzles 44 and venturis 37 in lieu of the single nozzle 44 and venturi 37.

As best shown in FIGS. 2 and 3, positioned in spaced relationship on the surface 30 of the burner tile 28 adjacent to the bottoms of the sections 36 and 38 of the wall 34 are a plurality of secondary fuel gas discharge nozzles 54. The nozzles 54 are positioned adjacent the intersections of the sections 36 and 38 with the surface of the base portion 30 of the burner tile 28. The nozzles 54 are connected to fuel gas conduits 56 (FIG. 2) which are connected to the fuel gas manifold 48 by unions 58. The nozzles 54 positioned adjacent to the sections 38 include fuel gas discharge openings therein whereby secondary fuel gas is discharged in fan shapes substantially parallel and adjacent to the sections 36 include fuel gas discharge openings therein whereby secondary fuel gas is discharged in fan shapes substantially parallel and adjacent to the exterior surfaces of the sections 36. As the secondary fuel gas discharged by the nozzles 54 flows over the surfaces of the sections 36 and 38, flue gases in the furnace space outside the burner tile 28 are mixed with the secondary fuel gas.

The passageways 42 in the sections 36 are positioned adjacent to the nozzles 54 as illustrated best in FIG. 3. In addition to the fuel gas discharge openings for discharging secondary fuel gas parallel to the surfaces of the sections 36, the fuel gas nozzles 54 adjacent to the sections 36 and the passageways 42 formed therein include primary fuel gas discharge openings for discharging primary fuel gas into the interior of the opening 32 and the wall 34 of the burner tile 28. Because of the primary fuel gas jets flowing through the openings 42, furnace space flue gases outside of the burner tile 28 are drawn into and flow through the openings 42 with the primary fuel gas into the interior of the opening 32 and wall 34 of the burner tile 28.

While the passageways 42 with primary fuel gas jets and flue gases flowing therethrough are preferably located in every other section as described above, it is to be understood that one or more passageways 42 with primary fuel gas jets and flue gases flowing therethrough can be utilized in the wall 34 of the burner tile 28.

In addition to defining the sections 36 and 38, the baffles function to divide the secondary fuel gas and flue gases into a plurality of separate streams which enter and intimately mix with the primary fuel gas-flue gases-air mixtures discharged from within the wall 34 of the burner tile 28. The primary fuel gas-flue gases-air mixtures formed within the wall 34 are ignited while within the wall 34 and then flow out of the wall 34. The collisions of the secondary fuel gas-flue gases streams with the primary fuel gas-flue gases-air mixtures create a plurality of U-shaped or folded flames 60 as shown in FIG. 5. As is well known by those skilled in the art, one of the primary mechanisms that produce NO<sub>x</sub> in a combustion process is thermal NO<sub>x</sub>, i.e., the higher the flame temperature, the more NO<sub>x</sub> that is created. In the burner apparatus of this invention, the multiplicity of folded flames 60 shown in FIG. 5 allow the fuel gas to be rapidly mixed with flue gases prior to and during burning with air thereby reducing NO<sub>x</sub>. Also, the increased surface area of the folded and convoluted flames 60 causes flue gases to mix with the flames more effectively, and the breaks 62 in the flames that exist between the folds allow flue gases to further penetrate between the flames and mix therewith, all of which contribute to very low NO<sub>x</sub> production.

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In operation of the burner apparatus 10, fuel gas is introduced into the furnace space to which the burner 10 is attached and burned therein at a flow rate which results in the desired heat release. Air is also introduced into the burner housing 14 and a column of the air flows into the furnace space. The flow rate of air introduced into the furnace space is in the range of from about 0% to about 100% in excess of the flow rate of air required to form a stoichiometric mixture of air and fuel gas. Preferably, the flow rate of air is in excess of the stoichiometric flow rate of air by about 15%. Stated another way, the mixture of fuel gas and air discharged into the furnace space contains from about 0% to about 100% of excess air. As shown in FIG. 2, the column of air flows through the housing 14 and through the opening 32 in the burner tile 28 into the mixing zone formed within the interior and above the wall 34. While within the mixing zone, the air mixes with the primary fuel gas and flue gases discharged into the mixing zone by way of the passageways 42 and the fuel gas nozzles 54 positioned adjacent to the passageways 42 and optionally by way of the fuel gas nozzle 44. The resulting primary fuel gas-flue gases-air mixture containing a

large excess of air is burned within and adjacent to the top of the burner tile 28 and the flue gases formed therefrom have very low NO<sub>x</sub> content due to the dilution of the fuel gas by the excess air and flue gases.

The secondary fuel gas discharged in directions parallel to the surfaces of the sections 36 and 38 by the nozzles 54 are mixed with flue gases surrounding the burner tile 28. The resulting secondary fuel gas-flue gases mixtures are discharged into the primary fuel gas-air mixture flowing from the interior of the wall 34 in a plurality of separate streams which form a folded flame pattern and mix with the primary fuel gas-air mixture to form a highly mixed fuel gas-flue gases-air mixture. The fuel gas-flue gases-air mixture burns in a multiplicity of folded flames in the furnace space and produces flue gases of low NO<sub>x</sub> content due to the fuel gas being diluted by relatively cool excess air and flue gases.

While the secondary fuel gas is preferably discharged by the nozzles 44 adjacent to the surfaces of all of the sections 36 and 38, it is to be understood that the secondary fuel gas can be discharged from one or more nozzles 44 adjacent to one or more of the sections 36 and 38.

A method of this invention for discharging a mixture of fuel gas and air into a furnace space wherein the mixture is burned in a folded flame pattern and flue gases having low NO<sub>x</sub> content are formed therefrom is comprised of the steps of: (a) discharging the air into a mixing zone within and adjacent to a wall which extends into the furnace space and has exterior sides divided into alternating sections by a plurality of radially positioned baffles attached thereto, the alternating sections having the same or different heights and slanting towards the opening at the same or different angles and one or more of the alternating sections having a passageway formed therein for conducting a primary fuel gas and flue gases mixture from outside the section to within the wall; (b) discharging a primary portion of the fuel gas from locations outside the wall and adjacent to the one or more wall sections having passageways formed therein so that the primary portion of the fuel gas is mixed with flue gases in the furnace space and the resulting primary fuel gas-flue gases mixture formed flows into the mixing zone within the wall by way of said passageways to form a primary fuel gas-flue gases air mixture which flows into the furnace space; and

(c) discharging a secondary portion of the fuel gas from one or more locations outside the wall and adjacent to one or more of the wall sections so that the secondary portion of fuel gas mixes with flue gases in the furnace space and the secondary fuel gas-flue gases mixture formed is discharged into the primary fuel gas-flue gases-air mixture in one or more separate streams formed by the radially positioned baffles which enter and mix with the primary fuel gas-flue gases-air mixture to form a highly mixed fuel gas-flue gases-air mixture which burns in the folded flame pattern.

The above method can also include the optional step of introducing a portion of the primary fuel gas into the mixing zone within the wall of the burner tile whereby the primary fuel gas mixes with air therein.

The fuel gas, flue gases and air discharged into the furnace space in accordance with step (b) can contain from about 0% to about 100% of excess air. The primary portion of fuel gas utilized in accordance with step (b) is in the range of from about 2% to about 40% by volume of the total fuel gas discharged into the furnace space and the secondary portion of fuel gas utilized in accordance with step (c) is in the range of from about 60% to about 98% by volume of the total fuel gas discharged into the furnace space.

Another method of this invention for discharging a fuel gas and air mixture into a furnace space wherein the mixture is burned in a folded flame pattern and flue gases having low NO<sub>x</sub> content are formed therefrom is comprised of the following steps: (a) discharging a column of the air into the furnace space; (b) discharging a first portion of the fuel gas mixed with flue gases from the furnace space into the column of the air; and (c) discharging a second portion of the fuel gas mixed with flue gases from the furnace space into the column of air containing the first portion of the fuel gas mixed with flue gases in a plurality of separate streams from spaced locations around the column, the separate streams entering the column radially and burning therein along with the first portion of the fuel gas in separate folded flames surrounded by and mixed with flue gases and air.

Yet another method of this invention for discharging a fuel gas and air mixture into a furnace space wherein the mixture is burned in a folded flame pattern and flue gases having low NO<sub>x</sub> content are formed therefrom is comprised of the following

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steps: (a) discharging said air into said furnace space; and (b) discharging said fuel gas mixed with flue gases from said furnace space into said air in two or more separate streams which enter the air and burn therein in one or more folded flames surrounded by and mixed with flue gases and air.

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In order to further illustrate the apparatus of this invention, its operation and the methods of the invention, the following examples are given.

#### **EXAMPLE 1**

A burner apparatus 10 designed for a heat release of 8,000,000 BTU per hour by burning natural gas having a caloric value of 913 BTU/SCF was fired into a furnace space. Pressurized fuel gas was supplied to the manifold 48 of the burner 10 at a pressure of about 33 psig and a flow rate of about 8765 SCF/hour. A 20% by volume portion of the fuel gas (1753 SCF/hour) was used as primary fuel gas and was discharged within the opening 32 and wall 34 of the burner tile 28 by the fuel gas discharge nozzle 44 and by the fuel gas discharge nozzles 54 positioned adjacent to the openings 42 in the wall 40 of the burner tile 28. The remaining portion of the fuel gas, i.e., the secondary portion (at a rate of 7012 SCF/hour) was discharged into the furnace space by the nozzles 54 in separate fuel gas streams mixed with flue gases.

The rate of air introduced into the furnace space by way of the air register 24, the housing 14 and the burner tile 28 was at least 15% in excess of the stoichiometric air rate relative to the total fuel gas rate. The primary fuel gas-flue gases air mixture began to burn at the vicinity of the passages 42 and at the top of the burner tile wall 34. The fuel gas-flue gases mixtures discharged at different angles into the partially burning fuel gas-air-flue gases mixture at the top of the burner tile wall 34 intimately mixed with flue gases from the furnace space and remaining air therein and burned above the burner tile in a short flame having a folded flame pattern. Because of the dilution of the primary and secondary fuel gases with flue gases and excess air and the intimate mixing of the fuel gas-air-flue gases mixture, the burner had a high turn down ratio and produced very low NO<sub>x</sub> emissions. Finally, the burner apparatus 10 has compact dimensions (significantly smaller than other low NO<sub>x</sub> burners) and can be easily installed in existing furnaces.

#### **EXAMPLE 2**

In order to see the flame pattern produced by the burner apparatus 10 when operated as described in Example 1 above, a computer simulation program was utilized. The software used was obtained from Fluent Inc. of Lebanon, New Hampshire. The design of the burner was reconstructed in the simulation program in full three dimensional detail including all important features such as tile facets, fuel gas port drillings, flame holder tile ledge and complete air plenum configuration.

A three dimensional model of the furnace in which the burner apparatus was tested was then prepared and the burner model was mounted in the furnace model exactly like the test burner and furnace utilized in Example 1 except that the air entered the housing from the side instead of the bottom. The flow spaces in the burner model were divided into small volumes using the finite volume method and boundary conditions were applied, e.g., fuel pressure, flow rates, etc. at the entrances of the burner model. The software then calculated and predicted the flow patterns as well as combustion reactions and the resulting flame pattern by iteratively calculating values for all the combustion and flow parameters in each of the small volumes.

The calculations were repeated until the predicted error was reduced to a desired level and then the output (a table of values for each volume) was fed into a graphics software package that produced a profile of static temperatures at planes cut through the flame at elevations of interest. One such elevation is presented in FIG. 5.

As shown in FIG. 5, the flame pattern includes eight folded flames 60 corresponding to the eight sections 36 and 38 of the burner tile having breaks 62 between the folds. The center flame 64 is produced by the burning of the fuel discharged from the fuel gas nozzle 44.

As mentioned previously herein, the separate folded flames 60 allow the fuel gas to be rapidly mixed with flue gases prior to burning with air thereby reducing the flame temperature and production of  $NO_x$ . Also, the increased surface of the folded flames 60 and the breaks 62 that exist between the folds allow flue gases to penetrate the flames and mix therewith to a greater degree than has heretofore been possible. Consequently, the  $NO_x$  emissions content of the flue gases released to the atmosphere is very low.

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Thus, the present invention is well adapted to carry out the objects and attain the ends and advantages mentioned as well as those which are inherent therein. While numerous changes may be made by those skilled in the art, such changes are encompassed within the spirit of this invention as defined by the appended claims.

What is claimed is: